# THE SOLUBILITY OF $\mathrm{CO}_{2}$ IN SOME $\mathrm{C}_{4}$ ALCOHOLS AT HIGH PRESSURES 


#### Abstract

I. Găinar* and Daniela Bala abstract: The aim of this work is to present the results concerning the solubility of $\mathrm{CO}_{2}$ in some $\mathrm{C}_{4}$ alcohols, namely $n$-butanole and iso-butanole by pressures up to 4 MPa and in temperature range $0 \div 40^{\circ} \mathrm{C}$. For both systems we observed remarkable values of gas solubility at all values of pressures and temperatures. Molecular structures of the alcohols have a small influence and therefore the obtained data are comparable. A different behaviour was observed at the lowest temperature and highest pressures for both alcohols. In these conditions the gas solubility exceeds the value 0.5 , it means that a new equilibrium is established: the solubility of liquid in the condensed gas.


## Introduction

The solubility of gases in liquids is an area of active interest from both the theoretical and practical standpoints. Both the dilute solutions resulting from the low solubility of many gases in liquids, and the large variety of sizes, shapes, and polarities of gases molecules to act as "probes" have made the solubility of gases in liquids an excellent tool to investigate the test theories of liquid properties and liquid structure. A knowledge of the solubility of gases is of practical importance in various industrial processes, in the study of artificial atmospheres for divers and astronauts, in the interaction of gases with our environment (as in the biological oxygen demand in natural waters), in processes for saline water demineralization, and in the study of various biological fluids and tissues.
Determination of the solubility of gases in liquids at high pressure has become of increasing importance. The problems of adequate mixing of the gas and liquid phases to ensure saturation, pressure and temperature control, and sampling and measurement of the gas dissolved at high-pressure present greater difficulties than in apparatuses that operate at atmospheric pressure.
The solubility of gases in liquids has been expressed in terms of many different units, depending on the particular application. The principal methods of expressing gas solubility are: the Bunsen coefficient $-\alpha$, the Kunsen coefficient - S, the Ostwald coefficient - L, the mole fraction $-x_{2}$, the absorption coefficient $-\beta$, the Henry's Law constant $-K_{H}$, the weight solubility $\mathrm{C}_{\mathrm{w}}[1,2]$.

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In our determinations we used mole fraction solubility $x_{2}$, which is given by:

$$
\begin{equation*}
x_{g}=x_{2}=\frac{n_{g}}{n_{g}+n_{s}} \tag{1}
\end{equation*}
$$

for two components, where $n$ is the number of moles (of gas and of solvent). The difficulty with this equation is that the gas solubility is directly proportional to the gas partial pressure via Henry's law. To be unambiguous then, both the partial pressure of the gas and the temperature of measurement must be specified to fix the mole fraction.
In this experiment we shall determine the solubility of $\mathrm{CO}_{2}$ in $n$-butanole and iso-butanole at pressures up to 4 MPa and in temperature range $0 \div 40^{\circ} \mathrm{C}$.
This work is a continuation of a programme initiated for some years ago concerning the solubility of gases in a wide category of organic solvents: hydrocarbons, alcohols, ketones at high pressure and a wide domain of temperatures [ $3 \div 5$ ].

## Materials and Methods

The experimental device and the detailed description of working method is presented in a separate research [6]. By using of this experimental method we have performed a study concerning the influence of temperature and pressure on gas solubility. In this purpose we have selected two alcohols namely $n$-butanole and iso-butanole. The used alcohols were Merck products and carbon dioxide was Linde gas one with high purity.
The measured experimental parameters were:

- working pressure (measured with a precision of $10^{-2} \mathrm{MPa}$ );
- working temperature (measured with a precision of $0.02^{\circ} \mathrm{C}$ );
- mass of alcohol (weighted with analytical balance);
- pressure of the desorbed gas (measured with a precision $\pm 0.005 \mathrm{~mm} \mathrm{Hg}$ ).


## Results and Discussion

Using the measured experimental parameters we calculate the moles number of the desorbed gas which represents the value of the carbon dioxide solubility in the given conditions of pressure and temperature. For the calculations the ideal gas equation was used, because the values of measured pressure did not exceed the values of working pressure. Other equations, as virial state equations were tested, but without any significant differences concerning the obtained values. The experimental data are presented in Table 1.

The pressure dependence of carbon dioxide solubility in n-butanole and iso-butanole is comparatively presented in Figs. $1 \div 6$.

Table 1. The solubility of carbon dioxide in $n$-butanole and iso-butanole at various temperatures

| n-butanole |  |  |  |  | iso-butanole |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\left(\begin{array}{c} \mathrm{t} \\ \left({ }^{\circ} \mathrm{C}\right) \end{array}\right.$ | $\begin{gathered} \mathbf{P}_{\text {working }} \\ (\mathrm{MPa}) \end{gathered}$ | $\begin{array}{\|c} \mathbf{m}_{\text {alcohol }}^{(\mathrm{g})} \end{array}$ | $\underset{\left(\mathrm{mm} \mathrm{Hg}_{\mathrm{Cg}}\right.}{\mathbf{P}^{2}}$ | $\mathrm{X}_{\mathrm{CO} 2}$ | $\mathbf{P}_{\text {working }}$ (MPa) | $\begin{gathered} \mathbf{m}_{\text {alcohol }} \\ (\mathrm{g}) \end{gathered}$ | $\underset{\left(\mathrm{mm} \mathrm{Hg}_{\mathrm{g})}\right.}{\mathbf{P}_{\mathrm{C}}}$ | $\mathrm{X}_{\mathrm{CO} 2}$ |
| 0 | $\begin{aligned} & 3.89 \\ & 3.19 \\ & 2.50 \\ & 2.01 \\ & 1.37 \\ & 0.78 \end{aligned}$ | $\begin{aligned} & 0.1881 \\ & 0.3427 \\ & 0.8068 \\ & 1.1403 \\ & 1.1319 \\ & 1.0623 \end{aligned}$ | $\begin{aligned} & 67.85 \\ & 56.55 \\ & 45.63 \\ & 44.75 \\ & 32.73 \\ & 23.55 \end{aligned}$ | $\begin{aligned} & 0.731 \\ & 0.554 \\ & 0.298 \\ & 0.228 \\ & 0.179 \\ & 0.143 \end{aligned}$ | $\begin{aligned} & 3.60 \\ & 3.09 \\ & 2.47 \\ & 2.06 \\ & 1.53 \\ & 1.08 \\ & 0.64 \end{aligned}$ | $\begin{aligned} & 0.2224 \\ & 0.5732 \\ & 0.8886 \\ & 1.0420 \\ & 1.1726 \\ & 1.4629 \\ & 1.4079 \end{aligned}$ | $\begin{aligned} & 94.70 \\ & 57.36 \\ & 48.81 \\ & 44.75 \\ & 36.60 \\ & 30.70 \\ & 16.70 \end{aligned}$ | $\begin{aligned} & 0.762 \\ & 0.429 \\ & 0.292 \\ & 0.244 \\ & 0.190 \\ & 0.136 \\ & 0.082 \end{aligned}$ |
| 10 | $\begin{aligned} & 4.49 \\ & 3.48 \\ & 2.35 \\ & 1.83 \\ & 1.25 \\ & 0.71 \end{aligned}$ | $\begin{aligned} & 0.2880 \\ & 0.5291 \\ & 1.0701 \\ & 1.0013 \\ & 1.1841 \\ & 1.8088 \end{aligned}$ | $\begin{aligned} & 43.90 \\ & 38.66 \\ & 41.64 \\ & 30.98 \\ & 24.81 \\ & 20.55 \end{aligned}$ | $\begin{aligned} & 0.534 \\ & 0.355 \\ & 0.226 \\ & 0.189 \\ & 0.136 \\ & 0.079 \end{aligned}$ | $\begin{aligned} & 3.53 \\ & 3.02 \\ & 2.59 \\ & 1.93 \\ & 1.47 \\ & 0.99 \\ & 0.61 \end{aligned}$ | $\begin{aligned} & 0.4661 \\ & 0.6632 \\ & 0.8808 \\ & 1.1120 \\ & 1.4807 \\ & 1.3469 \\ & 1.6989 \end{aligned}$ | $\begin{aligned} & 36.24 \\ & 37.16 \\ & 37.75 \\ & 35.50 \\ & 30.95 \\ & 19.30 \\ & 13.67 \end{aligned}$ | 0.369 0.296 0.244 0.194 0.136 0.097 0.057 |
| 20 | $\begin{gathered} 4.53 \\ 4.13 .04 \\ 3.44 \\ 2.52 \\ 1.98 \\ 0.73 \end{gathered}$ | $\begin{aligned} & 0.4976 \\ & 0.7436 \\ & 0.6039 \\ & 0.9372 \\ & 0.9842 \\ & 1.3697 \end{aligned}$ | $\begin{aligned} & 34.70 \\ & 45.01 \\ & 33.40 \\ & 31.95 \\ & 28.31 \\ & 14.41 \end{aligned}$ | $\begin{aligned} & 0.344 \\ & 0.313 \\ & 0.294 \\ & 0.204 \\ & 0.178 \\ & 0.073 \end{aligned}$ | $\begin{aligned} & \hline 4.31 \\ & 3.48 \\ & 3.02 \\ & 2.51 \\ & 1.98 \\ & 1.44 \\ & 0.94 \\ & 0.51 \end{aligned}$ | 0.7054 0.7715 0.8282 0.9417 0.9361 1.3774 1.3229 1.7541 | $\begin{aligned} & \hline 51.01 \\ & 40.27 \\ & 35.70 \\ & 32.25 \\ & 24.47 \\ & 25.83 \\ & 19.46 \\ & 14.29 \end{aligned}$ | $\begin{aligned} & \hline 0.352 \\ & 0.282 \\ & 0.245 \\ & 0.205 \\ & 0.164 \\ & 0.124 \\ & 0.100 \\ & 0.058 \end{aligned}$ |
| 25 | $\begin{aligned} & 4.28 \\ & 3.53 \\ & 2.50 \\ & 1.43 \\ & 1.02 \\ & 0.54 \end{aligned}$ | $\begin{aligned} & 0.7591 \\ & 0.8513 \\ & 1.2887 \\ & 1.5147 \\ & 1.6042 \\ & 1.2789 \end{aligned}$ | $\begin{aligned} & 39.62 \\ & 38.10 \\ & 37.31 \\ & 31.33 \\ & 28.50 \\ & 16.18 \end{aligned}$ | $\begin{aligned} & 0.282 \\ & 0.252 \\ & 0.179 \\ & 0.135 \\ & 0.118 \\ & 0.090 \end{aligned}$ | $\begin{aligned} & 3.48 \\ & 2.92 \\ & 2.41 \\ & 1.94 \\ & 1.46 \\ & 1.03 \\ & 0.57 \end{aligned}$ | $\begin{aligned} & 0.7300 \\ & 0.7015 \\ & 1.2836 \\ & 1.5712 \\ & 1.4869 \\ & 1.2581 \\ & 1.5429 \end{aligned}$ | 35.50 29.00 38.50 36.20 25.08 16.05 13.05 | $\begin{aligned} & 0.268 \\ & 0.237 \\ & 0.184 \\ & 0.148 \\ & 0.113 \\ & 0.088 \\ & 0.060 \end{aligned}$ |
| 30 | $\begin{aligned} & 4.27 \\ & 4.10 \\ & 3.35 \\ & 2.45 \\ & 1.78 \\ & 1.16 \\ & 0.67 \end{aligned}$ | $\begin{aligned} & 0.8738 \\ & 0.7489 \\ & 1.1284 \\ & 1.6610 \\ & 1.7915 \\ & 1.4820 \\ & 2.0241 \end{aligned}$ | $\begin{aligned} & 42.83 \\ & 33.71 \\ & 41.27 \\ & 42.05 \\ & 32.07 \\ & 19.82 \\ & 16.35 \end{aligned}$ | $\begin{aligned} & 0.269 \\ & 0.253 \\ & 0.216 \\ & 0.160 \\ & 0.119 \\ & 0.091 \\ & 0.057 \end{aligned}$ | $\begin{aligned} & 3.54 \\ & 2.98 \\ & 2.62 \\ & 1.99 \\ & 1.55 \\ & 1.03 \\ & 0.53 \end{aligned}$ | 0.5798 0.7647 0.6351 1.1885 1.3065 1.6634 1.6975 | $\begin{aligned} & 28.50 \\ & 29.12 \\ & 22.45 \\ & 28.68 \\ & 23.62 \\ & 21.20 \\ & 12.30 \end{aligned}$ | $\begin{aligned} & 0.270 \\ & 0.223 \\ & 0.200 \\ & 0.154 \\ & 0.120 \\ & 0.087 \\ & 0.052 \end{aligned}$ |
| 40 | $\begin{aligned} & 4.45 \\ & 3.45 \\ & 2.43 \\ & 1.51 \\ & 0.74 \end{aligned}$ | $\begin{aligned} & 0.9527 \\ & 1.1118 \\ & 1.6702 \\ & 1.2146 \\ & 1.3803 \end{aligned}$ | $\begin{aligned} & 39.37 \\ & 36.77 \\ & 37.09 \\ & 15.98 \\ & 11.53 \end{aligned}$ | $\begin{aligned} & 0.237 \\ & 0.199 \\ & 0.143 \\ & 0.090 \\ & 0.059 \end{aligned}$ | $\begin{aligned} & 3.22 \\ & 2.65 \\ & 2.14 \\ & 1.67 \\ & 1.08 \\ & 0.54 \end{aligned}$ | $\begin{aligned} & 0.8361 \\ & 0.9634 \\ & 1.1823 \\ & 1.7799 \\ & 1.2458 \\ & 1.9400 \end{aligned}$ | $\begin{aligned} & 28.43 \\ & 27.72 \\ & 25.10 \\ & 32.32 \\ & 15.18 \\ & 12.00 \end{aligned}$ | $\begin{aligned} & 0.204 \\ & 0.178 \\ & 0.138 \\ & 0.120 \\ & 0.084 \\ & 0.044 \end{aligned}$ |



Fig. 1. The pressure dependence of $\mathrm{CO}_{2}$ solubility in $n$-butanole and i-butanole at $0^{\circ} \mathrm{C}$


Fig. 3. The pressure dependence of $\mathrm{CO}_{2}$ solubility in $n$-butanole and i-butanole at $20^{\circ} \mathrm{C}$


Fig. 5. The pressure dependence of $\mathrm{CO}_{2}$ solubility in $n$-butanole and i-butanole at $30^{\circ} \mathrm{C}$


Fig. 2. The pressure dependence of $\mathrm{CO}_{2}$ solubility in $n$-butanole and i-butanole at $10^{\circ} \mathrm{C}$


Fig. 4. The pressure dependence of $\mathrm{CO}_{2}$ solubility in $n$-butanole and i-butanole at $25^{\circ} \mathrm{C}$


Fig. 6. The pressure dependence of $\mathrm{CO}_{2}$ solubility in n-butanole and i-butanole at $40^{\circ} \mathrm{C}$

## Conclusions

Analyzing the above results we obtained the following conclusions:

- at high pressures (greater than 3-4 MPa) and low temperature, $0^{0}$ and $10^{\circ} \mathrm{C}$ respectively, the solubility have great values. In these conditions the gas solubility exceeds the value 0.5 (as we can see from Table 1) and a new equilibrium is established: the solubility of liquid in the condensed gas. The liquid phase disappeared and in the working cell we have one phase with fog aspect;
- decreasing the pressure, the equilibrium curves change their slopes and at molar fractions smaller than 0.3 the pressure dependence of solubility becomes linear, it means that Henry's Law can be applied (see Fig. 1). At $10^{\circ} \mathrm{C}$ the phenomenon is less visible, but still we can remark the slope changing in $n$-butanole (see Fig. 2);
- increasing the temperature, the pressure dependence of solubility becomes linear on the entire range of values, it means that the Henry's Law is respected (Fig. 3 - Fig. 6).


## REFERENCES

1. Wilhelm, E. and Battino, R. (1971) J. Chem. Thermodyn. 3, 359.
2. Rettich, T., Battino, R. and Wilhelm, E. (1982) Ber. Bunsenges. Phys. Chem. 86, 1128.
3. Vîlcu, R., Găinar, I., Maior, O. and Anițescu, G. (1992) Rev. Roumanie Chim. 37, 875-8.
4. Vîlcu, R., Găinar, I., Anițescu, G. and Perişanu, S. (1991) Rev. Roumanie Chim. 36, 421-7.
5. Vîlcu, R., Găinar, I., Anițescu, G. and Perişanu, S. (1993) Rev. Roumanie Chim. 38, 1169-72.
6. Găinar, I. and Anițescu, G. (1995) Fluid Phase Equil. 109, 281-9.

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